STRATEGIZE YOUR STEAM SYSTEMS
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Irrespective of how steam is produced in our process plants, several aspects of steam generation are common; we should apply standard best practices to them. This column specifically addresses the blowdown stream as well as both the flash steam recovery and heat recovery that we should implement in our steam systems.

Every steam system has a water treatment plant; feedwater is made up of treated make-up water, returned condensate and directly injected steam (in the deaerator). Although the condensate and steam are clean, the treated makeup water still brings in dissolved impurities. Because these impurities are not soluble in steam, they remain in the boiler. As a result, their concentration builds and can lead to serious operational problems such as scaling on the water-side of the tubes resulting in tube leaks and failures, foaming resulting in liquid carryover, loose sludge in the boiler water, etc. All of these problems could damage boiler integrity. Blowdown is the primary mechanism that controls the water chemistry of the boiler water. It regulates the concentration of dissolved and precipitated chemicals in the boiler and, thus, ensures steam generation equipment functions reliably.

Generally, boiler water conductivity or total dissolved solids is used to control blowdown, but as our steam systems get more complex, other parameters — pH, silica, iron, etc. — also are used as secondary control points. In the past 25 years, I have seen blowdown rates as low as 1% and in some instances as high as 15%. Blowdown rate depends on several factors; however, I will not be covering blowdown rate in this column. Please work...
with your water chemist to ensure you have everything in place to minimize blowdown.

**CAPTURE THERMAL ENERGY**

Blowdown, because it is saturated liquid water at steam generation pressure, contains a significant amount of thermal energy. The higher the steam generation pressure, the higher the saturation (blowdown) temperature and the higher the thermal energy (Btu/lb) associated with the blowdown. As blowdown is discharged from the boiler, this thermal energy (provided by the fuel or from another source) is lost. Therefore, reducing the amount of blowdown to the bare minimum is an excellent best practice; beyond that we need to look at other mechanisms to capture lost energy.

So, that brings us to creating and recovering flash steam from blowdown and then, if economically justifiable, recovering heat from the liquid water before discharge. The simplest configuration is to first take the blowdown stream into a flash tank whose pressure is slightly higher than either the deaerator pressure or the lowest-pressure steam header in the steam generation area. The blowdown flashes and produces low-pressure steam that can be recovered and used within the steam system to offset deaerator steam demand. Recovering flash steam accounts for 65–70% of the total blowdown stream energy that would otherwise have been lost. Interestingly, the flash tank is a simple piece of equipment with no moving parts. On several occasions, I have been able to source it from within a plant’s operations that are no longer in service. The remainder of the liquid water from the flash tank is still hot (>225°F) and can be used to exchange heat in a simple one-pass shell-and-tube heat exchanger or a plate-and-frame unit, etc. This can be used to heat the makeup water going to the deaerator, thereby saving on overall steam demand from utilities.

Also, I have faced some challenges in plants when I tried implementing blowdown thermal energy recovery. Most relate to past incorrect applications, such as a large U-tube heat exchanger used to recover heat from blowdown that fouled and eventually was taken out of service because it became a maintenance headache. In other plants, because there is so much excess low-pressure steam, managers claim there’s no benefit of low-pressure, low-temperature heat recovery. This is not necessarily true; technologies exist to upgrade low-pressure steam and make use of every Btu that would otherwise be lost. I realize the overall blowdown energy recovery and cost savings may not be huge (<2%) but, as one of the simplest and most cost-effective best practices, it should never be ignored! (For more on improving boiler management to help save energy, see “Optimize Boiler Loads,” http://goo.gl/z9c1M1 and “Don’t Get Steamed,” http://goo.gl/xoUQSM.)

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Steam generation plays a critical role at many industrial facilities. Unfortunately, the high-temperature and high-pressure environment of large steam generators makes them susceptible to corrosion. Even seemingly minor impurity ingress can cause problems [1]. Fortunately, plants can take advantage of a lot of lessons learned about preventing corrosion in boilers. However, an often overlooked issue is the risk of severe corrosion occurring during those times when a steam generator is down due to lack of steam demand or for maintenance. This article outlines several techniques for protecting steam generators at these times. Our examples come from a power plant, Lincoln Electric System’s Terry Bundy Generating Station in Lincoln, Nebraska, but the technologies suit process plants as well.

**BACKGROUND**

The Terry Bundy plant has three GE LM6000 combustion turbines, two of which are equipped with heat recovery steam generators (HRSGs) that drive a supplemental steam turbine. Total plant capacity is 170 MW. The units cycle on and off, often on a daily basis during the summer, according to the requirements of the South West Power Pool. At other times, a unit may be down for several days or perhaps even weeks during periods of mild weather or for maintenance outages.

For normal operating chemistry, the HRSG feedwater is on an all-volatile treatment oxidizing [AVT(O)] program, with ammonium hydroxide injection to maintain feedwater pH within a 9.6–10 range. High-pressure evaporator chemistry complies with the...
Electric Power Research Institute’s phosphate guidelines, with trisodium phosphate as the only phosphate species and control within a 1–3 ppm range. The high-pressure evaporator pH control range is 9.5–10. Free caustic concentrations are maintained at or below 1 ppm to minimize the risk of caustic gouging.

For short-term outages, the HRSGs must remain full of condensate to enable quick startup. On the other hand, a maintenance outage requires draining of the unit, preferably while it is hot so it flash-dries. However, even such drying still leaves some areas exposed to moist conditions and, thus, vulnerable unless additional protective methods are used.

The equipment and processes outlined below all are designed to protect the unit from oxygen corrosion during any outage. Oxygen attack is extremely serious.

The corrosion mechanism can induce severe metal loss in those areas of high oxygen concentration. The attack often takes the form of pitting (Figure 1), where the concentrated corrosion can cause through-wall penetration and equipment failure in a short period of time.

In addition, oxygen attack will generate corrosion products that then carry over to the steam generator during startups. Deposition of iron oxides in the waterwall tubes leads to loss of thermal efficiency and, most importantly, establishes sites for under-deposit corrosion, such as very insidious hydrogen damage, acid phosphate corrosion (in units with poorly maintained or monitored chemistry — see: “Don’t Get Steamed,” http://goo.gl/XPhl7s), and caustic gouging [2].

Oxygen also can infiltrate steam generators at startup when collected condensate or fresh demineralized water is needed for filling or boiler top-off. These high-purity waters typically are stored in atmospherically vented tanks. The water absorbs oxygen and carbon dioxide, often to the saturation point, which may be up to 8 ppm in the case of oxygen. When the makeup is injected into a cold steam generator, significant oxygen attack is possible.

KEY MEASURES
To prevent oxygen ingress and corrosion, the Terry Bundy combined-cycle plant relies on four of the best techniques: nitro-
Nitrogen blanketing; periodic water circulation; dissolved oxygen removal from makeup condensate and demineralized water; and warm air recirculation to protect the low-pressure turbine.

Nitrogen blanketing. The first and foremost measure is nitrogen blanketing during shutdown and subsequent short-term layups. Experience has shown that introducing nitrogen to key points in the system before the pressure has totally decayed will minimize ingress of air. Then, as the system continues to cool, only nitrogen enters, not oxygen-laden air. Key points for nitrogen protection in HRSGs include the evaporator, economizer and feedwater circuits.

The nitrogen blanketing system was installed in 2005, just a few years after the steam generators’ startup, when plant personnel discovered oxygen pitting in one of the high-pressure evaporators as well as other corrosion.

One question that often arises is how best to supply nitrogen. Certainly local gas-supply or welding firms can provide bottles of compressed nitrogen. Liquid nitrogen is another possibility. Terry Bundy personnel selected a different method, nitrogen generation via a pressure-swing adsorption (PSA) system. (For more on such units for nitrogen generation, see: “Rethink Nitrogen Supply for Chemical Blanketing,” http://goo.gl/btiSw3.)

The process relies on a carbon molecular sieve that, when compressed air is introduced at high pressure, adsorbs oxygen, carbon dioxide and water vapor but allows nitrogen to pass through (Figure 2). The nitrogen then can be collected in a receiver for use as needed. At a preselected interval, pressure is released from the unit; O₂, CO₂, and H₂O desorb from the material and are vented to atmosphere. The nitrogen purity from this system depends upon production rate, and ranges from 1,000 scfh at 99.5% purity to 248 scfh at 99.99% purity.

The Terry Bundy N₂ generator supplies 5-psig nitrogen to the low-pressure and high-pressure drums during wet layups; the nitrogen also serves to “push” water from an HRSG during dry layup draining. A nitrogen pressure of 5 psig is maintained during the dry layup, provided no major tube work is required.
An obvious major concern with nitrogen blanketing — and why some plants don’t use it — is safety. Nitrogen is an asphyxiating agent and requires strict adherence to confined-space entry procedures and proper ventilation of the space.

*Periodic water circulation.* This is another important point with regard to wet layup chemistry. Regular water movement minimizes stagnant conditions that can concentrate oxygen in localized areas to cause pitting. Both Terry Bundy HRSGs have circulating systems installed on the high- and low-pressure circuits for use during wet layups. Each circuit uses one of two redundant preheater recirculation pumps, which normally are in service during HRSG operation to mitigate acid dew point corrosion of external circuits. Each pump provides approximately 100 gpm per circuit. Valves and piping have been added to enable seamless transition from layup circulation to normal operation. Sample/injection systems allow operators to test the layup chemistry for pH and dissolved oxygen (using colorimetric ampules), and to inject ammonium hydroxide if the pH must be raised. In addition, modifications made in each boiler drum permit the layup water to bypass the drum baffle, promoting circulation and minimizing short-circuiting via the downcomers. The pumps typically are started once drum pressure drops below 50 psig, and remain in service for the duration of the layup.

**Dissolved oxygen removal from condensate and makeup water.** Because demineralized water commonly is stored in atmospherically vented tanks, oxygen-laden water enters the steam generator during normal operation and, even more critically, during boiler filling. In the latter case, the influx of cold oxygen-saturated water can cause severe difficulties. One possible method to minimize this problem is to limit oxygen ingress to storage tanks — but this typically is a difficult proposition. So, instead, Terry Bundy personnel selected a gas-transfer membrane technology to treat condensate return and makeup water (Figure 3).

The oxygen-laden water flows along hollow-fiber membranes that let dissolved gases pass through but not the water. A sweep gas, often nitrogen, flows along the opposite surface of the membranes and carries away the gases. The technology can reduce the
dissolved oxygen concentration from saturated conditions to less than 10 ppb.

**DON'T FORGET THE STEAM TURBINE**

Far too often in the power industry, plants allow the condenser hotwell to remain moist or even contain standing water during outages in which the condenser vacuum was broken and air entered the condenser and low-pressure turbine. The low-pressure blades in steam turbines typically collect salts that carry over with steam from boiler drums. The combination of a moisture-laden atmosphere and these salt deposits can foster pitting and stress corrosion cracking.

A very practical method to combat this corrosion, and the one adopted at Terry Bundy, is injection of desiccated air into the condenser during all but short-term, i.e., <72 h, layups. This system uses a desiccant wheel dehu-

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midifier (Figure 4) to provide 700 scfm of 100°F air at 10% humidity to the condenser and low-pressure turbine. This flow can lower the relative humidity from nearly 100% to less than 30% in just a few hours.

IMPRESSIVE RESULTS

In 2005, drum inspections showed significant pitting. This prompted implementing the changes we’ve outlined. A repeat inspection in 2008 showed no new pitting (Figure 5). Subsequent inspections continue to show little to no additional pitting.

Iron level monitoring, via particulate collection on 0.45-micron filters, showed a significant decrease in samples from the condensate pump discharge and both low-pressure and high-pressure drums. Quicker startups than in the past are now commonplace. In addition and of significant importance, the units can be left in wet layup for extended periods, which saves the plant six hours (over dry layup) to reach full load when needed.

FOLLOW-UP INSPECTION

Figure 5. Check conducted three years after measures were implemented showed no new pitting. Source: Lincoln Electric System.

REFERENCES


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Refineries and other chemical plants frequently miss or have a delayed response to critical issues in daily operations due to failed steam traps. However, failed steam traps are often viewed as a routine part of running a plant or the cost of production. While steam traps play a crucial role in plantwide safety, equipment reliability and product quality, they also can cause production interruptions if not maintained properly.

**STEAM SYSTEM CHALLENGES**

Refineries often experience daily issues due to a lack of steam system and steam trap management. Some of the problems encountered include:

- Injuries and incidents related to steam tracing
- Escalating repair costs
- Increasing unit freeze-up issues
- The inability to distinguish easily between working and nonworking steam traps
- The inability to generate work lists for repairs resulting from an incomplete database
- Inappropriate or insufficient repair tracking

Steam trap management can be a cumbersome task for refineries that house 2,000 to 10,000 traps, so the ability to manage steam traps while generating data collection is advantageous. Without a steam system management tool, refineries are unable to generate reports for failed traps or seasonal shutoffs or provide reports by area or site. They also have no access to consistent information in real time.
Steam system monitoring software can help refineries keep a close eye on their steam traps. The software uses algorithms to analyze steam trap data to track behavior and performance for steam system management. It tests, records, tracks and reports on plant steam systems so that refineries and other chemical plants can manage multiple sites and various steam trap types while decreasing the overall time required for data collection, recording and reporting.

**MONITORING STEAM TRAPS**

To address such issues, a U.S. refinery with a capacity of 125,000 bbl/d of crude oil turned to Sage for help with managing 9,010 steam traps. Within the first six to eight months of starting the program, the refinery documented savings of more than $5 million as well as reductions in energy and steam costs.

The software is designed to be intuitive to use and easily accessible by an exclusive mobile app (Figure 1). It offers tight security, instant notifications and precise documentation and can accommodate companies of any size. It allows refineries to increase equipment reliability, efficiency and safety, while enabling reductions in environmental emissions. Reports generated provide a totalized summary of selected data in any of the following categories: monetary loss, fuel used, repair cost, payback period, and CO₂ emissions.

The software’s Team System, provides a facility summary of steam trap system performance rate and daily losses. It also alerts users with system notifications that allow for easy identification of problems and maintenance of equipment. It also shows annual steam loss — a 12-month view of steam and monetary loss (Figure

**MOBILE APP**

Figure 1. Steam system management can be carried out from the palm of your hand. This screen shows which traps have been tested along with pictures and trap conditions.
Look for steam trap monitoring technology that offers features such as these that may be beneficial to refineries:

- Cloud-based data that provides access to historical information for all steam traps as needed, by individual location or area, for multiple sites, with no need to load specific routes;
- Steam trap failure prediction based on historical data;
- Determine of the most appropriate steam trap for an application or unique conditions of a certain area;
- Inventory, categorization and tracking of the entire steam trap population;
- Surveying, tagging and identification of steam traps and in-house surveys and partial surveys of the traps, including photos of individual traps;
- Repair list generation;
- Active steam trap testing;
- Seasonal steam trap viewing and identification of traps to be shut off;
- CO₂ footprint monitoring.

REFINERY SEES INCREASED EFFICIENCIES

The refinery now has access to the right information at the right time and by the right people. The software improved the refinery’s ability to find and repair steam leaks, including those not associated with steam traps, and, as a result, it has reduced its steam trap failure rate significantly. The refinery’s required steam production also has been reduced substantially, and the steam system runs with increased efficiency and less waste.

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